

Hazards, Accidents, Process Safety Management & Process Hazard Analysis

*“As if there were safety in
stupidity alone.” – Thoreau*

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significant material from SACHE 2003 Workshop

Lecture Topics

- Hazards and Accidents
- Process Safety Management (PSM)
- Process Hazard Analysis (PHA)

Learning Objectives

- Describe the hazard and accident-driven stimulus for, and main components of OSHA's *Process Safety Management* standard
- Define *Process Hazard Analysis* and related terminology
- Describe major hazard analysis methods
- Assess applicability (via pros and cons) of major hazard analysis methods

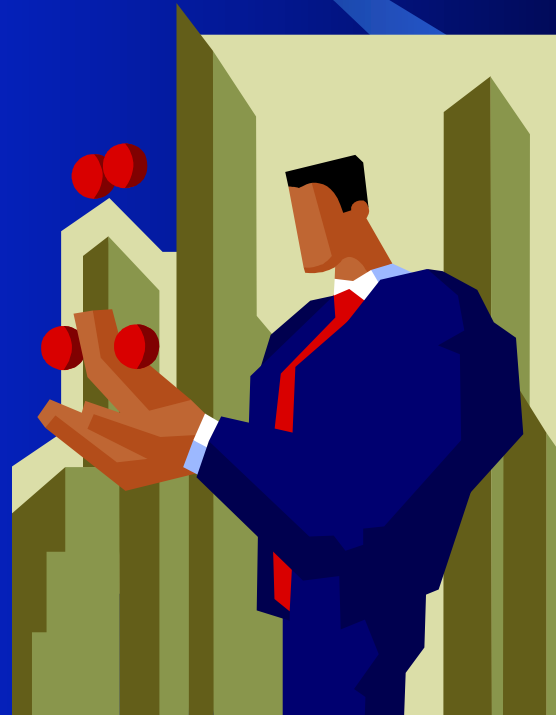
Hazards

- An inherent physical or chemical characteristic that has the potential for causing harm to people, the environment, or property¹
- Hazards are intrinsic to a material, or its conditions of use
- Examples
 - Hydrogen sulfide – toxic by inhalation
 - Gasoline – flammable
 - Moving machinery – kinetic energy, pinch points

¹ AICHE Center for Chemical Process Safety

Hazard Management: The World as It Was Before

- Good people
- ... doing good things



The Rising Case for Change

- 1984 – Bhopal, India – Toxic Material Released

- 2,500 immediate fatalities; 20,000+ total
- Many other offsite injuries



The Rising Case for Change

- 1984 – Mexico City, Mexico – Explosion
 - 300 fatalities (mostly offsite)
 - \$20M damages



The Rising Case for Change

- 1988 – Norco, LA – Explosion
 - 7 onsite fatalities, 42 injured
 - \$400M+ damage



The Rising Case for Change

- 1989 – Pasadena, TX – Explosion and Fire
 - 23 fatalities, 130 injured; damage \$800M+



Enter ... Process Safety Management

- Integral part of OSHA Occupational Safety and Health Standards since 1992
- Known formally as: *Process Safety Management of Highly Hazardous Chemicals* (29 CFR 1910.119)
- *PSM* applies to most industrial processes containing 10,000+ pounds of hazardous material

In a Few Words, What is PSM?

- The *proactive* and *systematic* identification, evaluation, and mitigation or prevention of chemical releases that could occur as a result of failures in process, procedures, or equipment.



What's Covered by PSM?

- Process Safety Information
- Employee Involvement
- Process Hazard Analysis
- Operating Procedures
- Training
- Contractors
- Pre-Startup Safety Review
- Mechanical Integrity
- Hot Work
- Management of Change
- Incident Investigation
- Emergency Planning and Response
- Compliance Audits
- Trade Secrets

Process Hazard Analysis

Simply, PHA allows the employer to:

- Determine locations of potential safety problems
- Identify corrective measures to improve safety
- Preplan emergency actions to be taken if safety controls fail

PHA Requirements

- Use one or more established methodologies appropriate to the complexity of the process
- Performed by a team with expertise in engineering and process operations
- Includes personnel with experience and knowledge specific to the process being evaluated and the hazard analysis methodology being used

PHA Must Address ...

- The hazards of the process
- Identification of previous incidents with likely potential for catastrophic consequences
- Engineering and administrative controls applicable to the hazards and their interrelationships

PHA Must Address ... (cont'd)

- Consequences of failure of engineering and administrative controls, especially those affecting employees
- Facility siting; human factors
- The need to promptly resolve PHA findings and recommendations

Hazard Analysis Methodologies

- What-If
- Checklist
- What-If/Checklist
- Hazard and Operability Study (HAZOP)
- Failure Mode and Effects Analysis (FMEA)
- Fault Tree Analysis
- An appropriate equivalent methodology

What-If

- Experienced personnel brainstorming a series of questions that begin, "What if...?"
- Each question represents a potential failure in the facility or misoperation of the facility

What-If

- The response of the process and/or operators is evaluated to determine if a potential hazard can occur
- If so, the adequacy of existing safeguards is weighed against the probability and severity of the scenario to determine whether modifications to the system should be recommended

What-If – Steps

1. Divide the system up into smaller, logical subsystems
2. Identify a list of questions for a subsystem
3. Select a question
4. Identify hazards, consequences, severity, likelihood, and recommendations
5. Repeat Step 2 through 4 until complete

What-If Question Areas

- Equipment failures
 - What if ... a valve leaks?
- Human error
 - What if ... operator fails to restart pump?
- External events
 - What if ... a very hard freeze persists?

What-If – Summary

- Perhaps the most commonly used method
- One of the least structured methods
 - Can be used in a wide range of circumstances
 - Success highly dependent on experience of the analysts
- Useful at any stage in the facility life cycle
- Useful when focusing on change review

Checklist

- Consists of using a detailed list of prepared questions about the design and operation of the facility
- Questions are usually answered “Yes” or “No”
- Used to identify common hazards through compliance with established practices and standards

Checklist Question Categories

- Causes of accidents
 - Process equipment
 - Human error
 - External events
- Facility Functions
 - Alarms, construction materials, control systems, documentation and training, instrumentation, piping, pumps, vessels, etc.

Checklist Questions

- Causes of accidents
 - Is process equipment properly supported?
 - Is equipment identified properly?
 - Are the procedures complete?
 - Is the system designed to withstand hurricane winds?
- Facility Functions
 - Is it possible to distinguish between different alarms?
 - Is pressure relief provided?
 - Is the vessel free from external corrosion?
 - Are sources of ignition controlled?

Checklist – Summary

- The simplest of hazard analyses
- Easy-to-use; level of detail is adjustable
- Provides quick results; communicates information well
- Effective way to account for ‘lessons learned’
- NOT helpful in identifying new or unrecognized hazards
- Limited to the expertise of its author(s)

Checklist – Summary (cont'd)

- Should be prepared by experienced engineers
- Its application requires knowledge of the system/facility and its standard operating procedures
- Should be audited and updated regularly

What-If/Checklist

- A hybrid of the What-If and Checklist methodologies
- Combines the *brainstorming* of What-If method with the *structured features* of Checklist method

What-If/Checklist – Steps

- Begin by answering a series of previously-prepared ‘What-if’ questions
- During the exercise, brainstorming produces additional questions to complete the analysis of the process under study

What-If/Checklist – Summary

- Encourages creative thinking (What-If) while providing structure (Checklist)
- In theory, weaknesses of stand-alone methods are eliminated and strengths preserved – not easy to do in practice
- E.g.: when presented with a checklist, it is typical human behavior to suspend creative thinking

HAZOP

Hazard and Operability Analysis

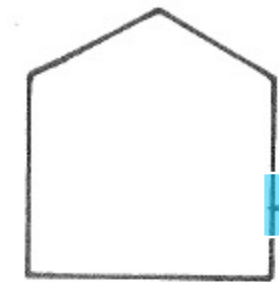
- Identify hazards (safety, health, environmental), and
- Problems which prevent efficient operation

HAZOP

1. Choose a vessel and describe intention
2. Choose and describe a flow path
3. Apply *guideword* to *deviation*
 - Guidewords include **NONE, MORE OF, LESS OF, PART OF, MORE THAN, OTHER THAN, REVERSE**
 - Deviations are expansions, such as **NO FLOW, MORE PRESSURE, LESS TEMPERATURE, MORE PHASES THAN** (there should be),

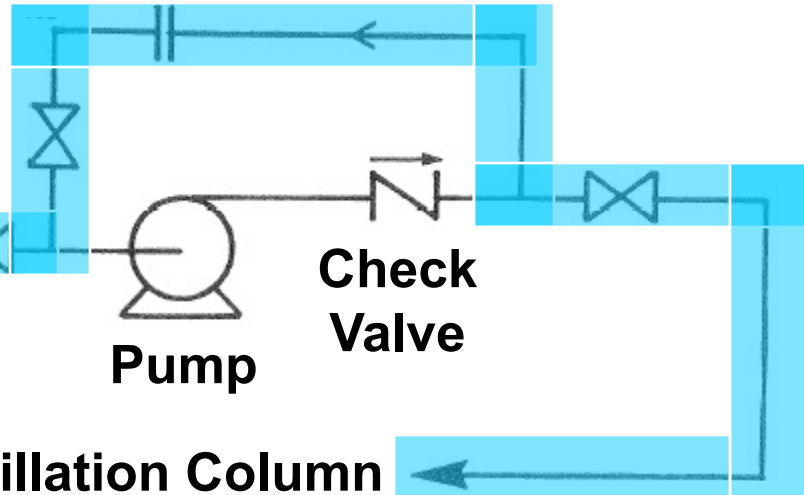
HAZOP

1. Vessel



Feed Tank

2. FLOW PATH

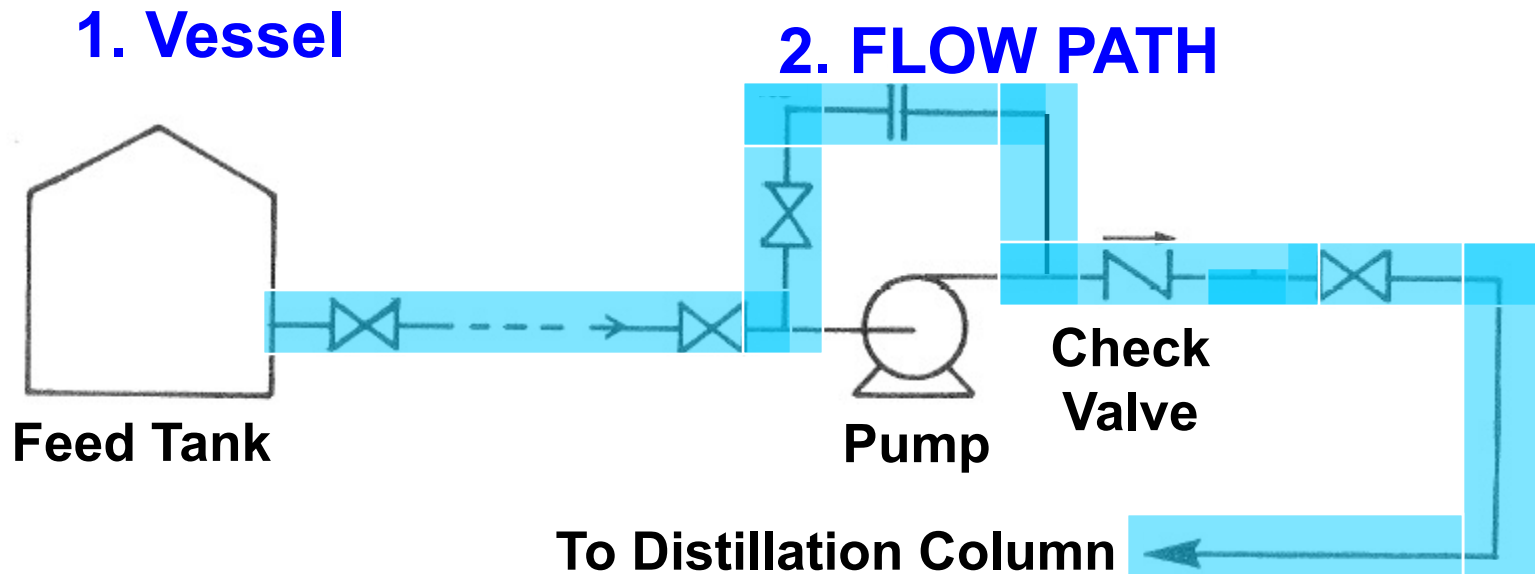


3. REVERSAL OF FLOW

HAZOP

4. Can deviation initiate a hazard of consequence?
5. Can failures causing deviation be identified?
6. Investigate detection and mitigation systems
7. Identify recommendations
8. Document
9. Repeat 3-to-8, 2-to-8, and 1-to-8 until complete

HAZOP



3. REVERSAL OF FLOW

- 4. Distillation materials returning via pumparound
- 5. Pump failure could lead to REVERSAL OF FLOW
- 6. Check valve located properly prevents deviation
- 7. Move check valve downstream of pumparound

Loss of Containment Deviations

- Pressure too high
- Pressure too low (vacuum)
- Temperature too high
- Temperature too low
- Deterioration of equipment

HAZOP's Inherent Assumptions

- Hazards are detectable by careful review
- Plants designed, built and run to appropriate standards will not suffer catastrophic *loss of containment* if ops stay within design parameters
- Hazards are controllable by a combination of equipment, procedures which are *Safety Critical*
- HAZOP conducted with openness and good faith by competent parties

HAZOP – Pros and Cons

- Creative, open-ended
- Completeness – identifies all process hazards
- Rigorous, structured, yet versatile
- Identifies safety *and* operability issues
- Can be time-consuming (e.g., includes operability)
- Relies on having right people in the room
- Does not distinguish between low probability, high consequence events (and vice versa)

FMEA – Failure Modes, Effects Analysis

- **Manual analysis** to determine the consequences of component, module or subsystem failures
- Bottom-up analysis
- Consists of a spreadsheet where each failure mode, possible causes, probability of occurrence, consequences, and proposed safeguards are noted.

FMEA – Failure Mode Keywords

- Rupture
- Crack
- Leak
- Plugged
- Failure to open
- Failure to close
- Failure to stop
- Failure to start
- Failure to continue
- Spurious stop
- Spurious start
- Loss of function
- High pressure
- Low pressure
- High temperature
- Low temperature
- Overfilling
- Hose bypass
- Instrument bypassed

FMEA on a Heat Exchanger

Failure Mode	Causes of Failure	Symptoms	Predicted Frequency	Impact
Tube rupture	Corrosion from fluids (shell side)	H/C at higher pressure than cooling water	Frequent – has happened 2x in 10 yrs	Critical – could cause a major fire

- Rank items by risk (frequency x impact)
- Identify safeguards for high risk items

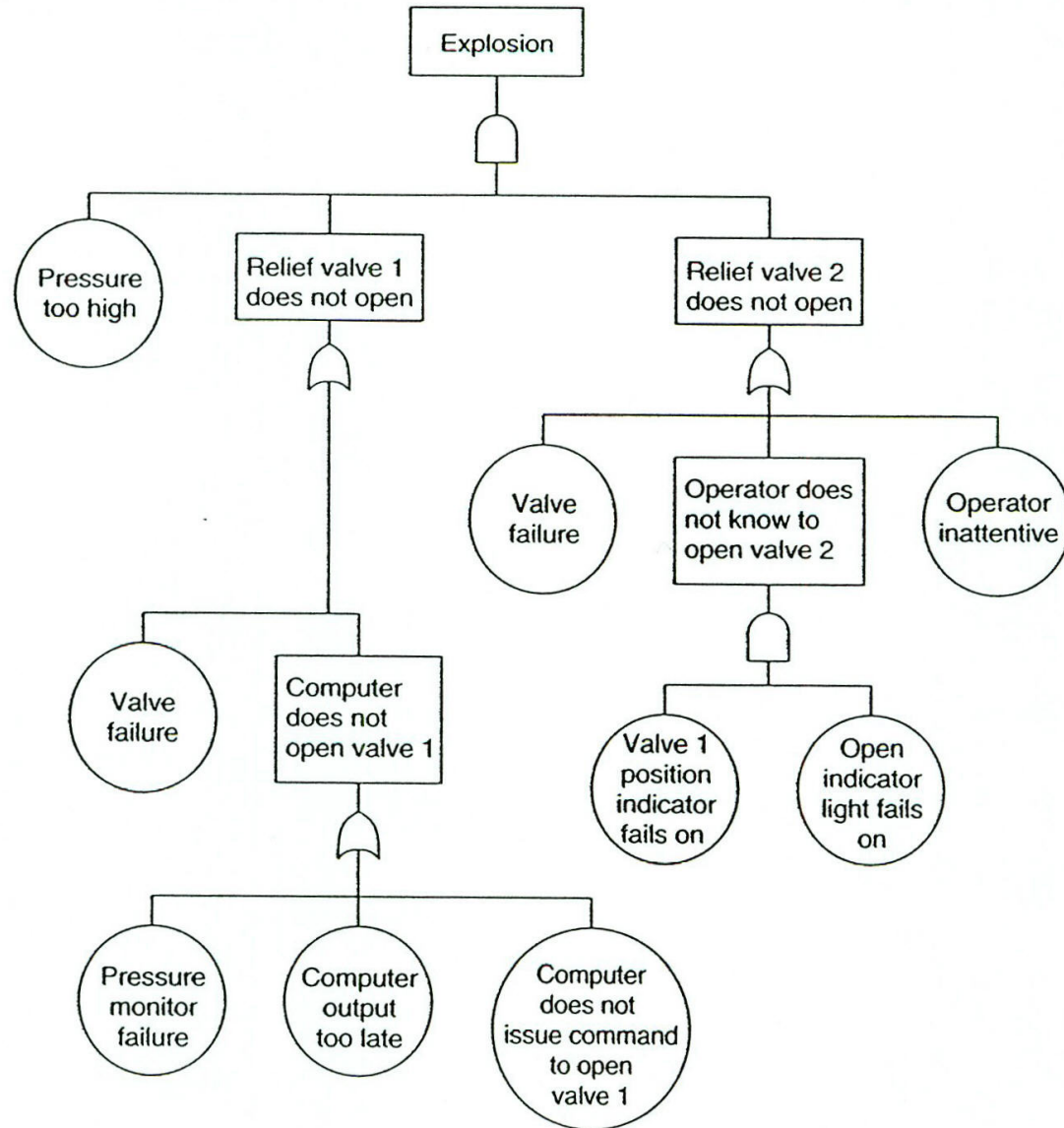
FMEA – Failure Modes, Effects Analysis

- FMEA is a very structured and reliable method for evaluating hardware and systems.
- Easy to learn and apply and approach makes evaluating even complex systems easy to do.
- Can be very time-consuming (and expensive) and does not readily identify areas of multiple fault that could occur.
- Not easily lent to procedural review as it may not identify areas of human error in the process.

Fault Tree Analysis

- **Graphical method** that starts with a hazardous event and works backwards to identify the causes of the *top event*
- Top-down analysis
- Intermediate events related to the top event are combined by using logical operations such as AND and OR.

FTA



Fault Tree Analysis

- Provides a traceable, logical, quantitative representation of causes, consequences and event combinations
- Amenable to – but for comprehensive systems, requiring – use of software
- Not intuitive, requires training
- Not particularly useful when temporal aspects are important

Accident Scenarios May Be Missed by PHA

- No PHA method can identify all accidents that could occur in a process
- A scenario may be excluded from the scope of the analysis
- The team may be unaware of a scenario
- The team consider the scenario but judge it not credible or significant
- The team may overlook the scenario

Summary

Despite the aforementioned issues with PHA:

- Companies that rigorously exercise PHA are seeing a continuing reduction in frequency and severity of industrial accidents
- *Process Hazard Analysis* will continue to play an integral role in the design and continued examination of industrial processes

Using What You Learn

- The ideas and techniques of Process Hazard Analysis will be immediately useful in upcoming recitation exercise on **Hazard Evaluation**
- Expect to be part of a Process Hazard Analysis Team early on in your professional career

Where to Get More Information

- Chemical Safety and Hazard Investigation Board's web site: *www.csb.gov*
- MPRI web site: *www.Mpri.lsu.edu/main/*
- Crawl and Louvar — *Chemical Process Safety: Fundamentals with Applications*
- Kletz — *HAZOP & HAZAN: Notes on the Identification and Assessment of Hazards*